Amendments to the Claims:

This listing of claims will replace all prior versions, and listings, of claims in the application.

Listing of Claims:

1-45. Cancelled.

- 46. (previously presented) A process for producing linear alkyl benzene, the process including the steps of obtaining a hydrocarbon condensate containing olefins, paraffins and oxygenates from a low temperature Fischer-Tropsch reaction;
 - a) fractionating a desired carbon number distribution from the hydrocarbon condensate to form a fractionated hydrocarbon condensate stream which is the product of a Fischer-Tropsch reaction;
 - b) extracting oxygenates from the fractionated hydrocarbon condensate stream from step (a) to form a stream containing olefins and paraffins which is the product of a Fischer-Tropsch reaction;
 - c) combining the stream containing olefins and paraffins from step (b), which is the product of a Fischer-Tropsch reaction, with the feed stream from step (g) to form a combined stream;
 - d) alkylating olefins in the combined stream from step (c) with benzene in the presence of a suitable alkylation catalyst in an alkylation reactor;
 - e) recovering linear alkyl benzene from the alkylation reactor;
 - f) recovering unreacted paraffins from the alkylation reactor;
 - g) dehydrogenating the unreacted paraffins in the presence of a suitable dehydrogenation catalyst to form a feed stream containing olefins and paraffins; and
 - h) sending the feed stream containing olefins and paraffins from step (g) to step (c).

Serial No. 10/549,768 Filed: September 11, 2006 Amendment

47. (previously presented) A process according to claim 46, wherein, in the extraction step b), the ratio of olefins to paraffins is substantially preserved.

- 48. (previously presented) A process according to claim 46, wherein the low temperature Fischer-Tropsch reaction is carried in a slurry bed reactor at a temperature of 160°C 280°C and in the presence of a cobalt catalyst to provide a hydrocarbon condensate containing 60 to 80% by weight paraffins and 10 to 30% by weight olefins.
- 49. (previously presented) The process according to claim 48, wherein the Fischer-Tropsch reaction is carried out at a temperature of 210°C 260°C.
- 50. (previously presented) The process according to claim 46, wherein the Fischer-Tropsch reaction is carried out in the presence of a cobalt catalyst.
- 51. (currently amended) The process according to claim 48, wherein the hydrocarbon condensate contains 10 to less than 25% by weight olefins.
- 52. (previously presented) The process according to claim 48, wherein the olefins in the hydrocarbon condensate have a linearity of greater than 92%.
- 53. (previously presented) The process according to claim 52, wherein the olefins in the hydrocarbon condensate have a linearity of greater than 95%.
- 54. (previously presented) The process according to claim 48, wherein the paraffins in the hydrocarbon condensate have a linearity greater than 92%.
- 55. (previously presented) The process according to claim 46, wherein the hydrocarbon condensate is fractionated, in step a), into the C₈ to C₁₆ range.
- 56. (previously presented) The process according to claim 55, wherein the hydrocarbon condensate product is fractionated, in step a), into the C_{10} to C_{13} range.

Serial No. 10/549,768 Amendment Filed: September 11, 2006

57. (previously presented) The process according to claim 56, wherein the fractionated hydrocarbon product contains 10 to 30% by weight olefins with a degree of linearity greater than 92%.

- 58. (previously presented) The process according to claim 46, wherein the oxygenates are extracted, in step (b), by distillation, dehydration or liquid-liquid extraction.
- 59. (previously presented) The process according to claim 58, wherein the oxygenates are extracted by liquid-liquid extraction.
- 60. (previously presented) The process according to claim 59, wherein a light solvent is used in the liquid-liquid extraction.
- 61. (previously presented) The process according to claim 60, wherein the light solvent is a mixture of methanol and water.
- 62. (previously presented) The process according to claim 61, wherein the oxygenate extraction process is a liquid-liquid extraction process that takes place in an extraction column using a mixture of methanol and water as the solvent, wherein an extract from the liquid-liquid extraction is sent to a solvent recovery column from which a tops product comprising methanol, olefins and paraffins is recycled to the extraction column, thereby enhancing the overall recovery of olefins and paraffins.
- 63. (previously presented) The process according to claim 62, wherein a bottoms product from the solvent recovery column is recycled to the extraction column.
- 64. (previously presented) The process according to claim 61, wherein the solvent has a water content of more than 3% by weight.

Serial No. 10/549,768 Filed: September 11, 2006

Amendment

65. (previously presented) The process according to claim 64, wherein the solvent has a water content of from 5% - 15% by weight.

- 66. (previously presented) The process according to claim 62, wherein a raffinate from the extraction column is sent to a stripper column from which a hydrocarbon feed stream containing more than 90% by weight olefins and paraffins and less than 0.2% by weight oxygenates exits as a bottoms product.
- 67. (previously presented) The process according to claim 66, wherein the hydrocarbon feed stream contains less than 0.02% by weight oxygenates.
- 68. (previously presented) The process according to claim 46, wherein the recovery of olefins and paraffins in the hydrocarbon feed stream over the extraction step b) is in excess of 70%.
- 69. (previously presented) The process according to claim 68, wherein the recovery of olefins and paraffins in the hydrocarbon feed stream is in excess of 80%.
- 70. (previously presented) The process according to claim 46, wherein the olefin/paraffin ratio of the fractionated hydrocarbon condensate stream a) is substantially preserved over the extraction step b).
- 71. (previously presented) The process according to claim 46, wherein the dehydrogenation reaction at step (g) is carried out at a conversion rate of 10%-15%.
- 72. (previously presented) The process according claim 71, wherein the fractionated hydrocarbon condensate from step (b) has an olefin concentration of from 10% to 30% by weight, the feed stream from step (g) has an olefin concentration of 10% to 15% by weight, and the combined stream at step (c) has an olefin concentration of 12.5% to 22.5% by weight.